

## Determination of Thermodynamic Properties of Gibbsite from Its Solubility Data in NaOH Solutions<sup>1)</sup>

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A reasonable method for determination of thermodynamic properties of alumina hydrates from their solubility data in alkaline pH range was presented and applied to the solubility data of gibbsite in NaOH solutions with success. When  $\log(K_s/a_w)$ , where  $K_s = m_H m_{Al}$  and  $a_w$  is the activity of water, was plotted against a Debye-Hückel function of the ionic strength  $I$ ,  $I^{1/2}/(1 + B_t a_1 I^{1/2})$ , a linear relationship to moderately high ionic strengths was found over the range of temperatures from 40 to 110 °C, having the theoretical Debye-Hückel limiting slope and the intercept of  $\log K_s^\circ$  at  $I=0$ . Assuming the same ionic size parameters,  $a_1 = a_2$ , the solubility product ( $K_s^\circ$ ) of gibbsite was found to depend upon temperature up to 110 °C as follows:  $\log K_s^\circ = -4064/T - 1.54$  or  $-4023/T - 1.65$ . At high ionic strengths above 1.0,  $\log(K_s/a_w)$  showed positive deviations from the straight line, which may be attributed to the formation of complex ions, e.g.,  $Al_2O(OH)_6^{2-}$ , or the dehydration of  $Al(OH)_4^-$  to  $AlO(OH)_2^-$  and  $AlO_2^-$  ions.

The solubility of alumina hydrates such as gibbsite, boehmite, and diasporite in aqueous solutions is very important not only for alumina production by the alkaline or acid process, but also for quantitative understanding of aqueous geochemistry of aluminous minerals.<sup>2-15)</sup> Furthermore, the thermodynamics of  $Al-H_2O$  system is much useful in considering the corrosion and passivation of aluminium in water.<sup>16)</sup> A number of solubility data of gibbsite in alkaline solutions have been reported by many investigators.<sup>2-13)</sup> A purpose of most previous solubility studies is to determine precisely the standard thermodynamic properties of gibbsite and hydroxy-aluminium ions in aqueous solutions. Unfortunately, these results do not agree well with each other; for example, as the ionic solubility product of gibbsite at 25 °C, Kittrick<sup>6)</sup> and May<sup>10)</sup> reported the values of  $5.01 \times 10^{-16}$  and  $8.94 \times 10^{-15}$ , respectively.

Russell, Edward and Taylor<sup>2)</sup> calculated an equilibrium constant ( $K_1$ ) and its temperature dependancy from their solubility data of gibbsite in NaOH solutions from 40 to 170 °C, assuming that activity coefficients of  $OH^-$  and  $AlO_2^-$  ions are equal to each other, i.e.,  $\gamma_{OH^-} = \gamma_{AlO_2^-}$ ;



$$K_1 = C_{Al} a_w^2 / C_{OH}, \quad (2)$$

$$\log K_1^\circ = -1605/T + 4.11, \quad (3)$$

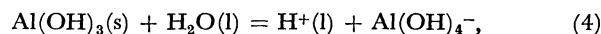
where  $C_{Al}$  and  $C_{OH}$  are the equivalents per liter of aluminate and hydroxide ions,  $a_w$  is the activity of the water in the molar fraction unit, and  $K_1^\circ$  is the value derived by extrapolating  $K_1$  to zero NaOH concentration at a given temperature. There are some doubtful problems in the Russell's method for determining  $K_1^\circ$ ; firstly, the differences in the ion size and interactions between the ions and water were neglected, assuming that the activity coefficients of  $AlO_2^-$  and  $OH^-$  ions are the same. Secondly, the values of  $a_w$  for NaOH solutions at 25 °C were used for sodium aluminate and hydroxide solutions at higher temperatures up to 170 °C without any correction. Finally the aluminate ion was expressed in the form of  $AlO_2^-$ .

The purpose of this work is to determine the thermodynamic properties of gibbsite in NaOH solution from its solubility data by a more reasonable method

according to the Debye-Hückel theory.

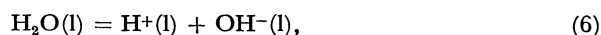
### Theoretical

According to various studies on the sodium aluminate and hydroxide solutions, the most probable structure of the aluminate ion is tetrahedral  $Al(OH)_4^-$  ion at low aluminium concentrations, which, at higher concentrations, becomes dehydrated  $AlO_2^-$  ion.<sup>17-19)</sup> Therefore, it is reasonable to express the dissolution process of gibbsite as follows;



$$K_s^\circ = a_H a_{Al} / a_w = K_s \cdot \gamma_1^2 / a_w, \quad (5)$$

where  $K_s = m_H m_{Al}$ ,  $\gamma_1^2 = \gamma_H \gamma_{Al}$ , and  $m_1$  is the molality of species  $i$ . On the other hand, for the dissociation of water,



$$K_w^\circ = a_H a_{OH} / a_w = K_w \gamma_2^2 / a_w, \quad (7)$$

where  $K_w = m_H m_{OH}$  and  $\gamma_2^2 = \gamma_H \gamma_{OH}$ . From Eqs. 5 and 7 a general equation (8) for alumina trihydrates can be derived, introducing a new function,  $f(I)$ , of ionic strength ( $I$ ).

$$\begin{aligned} f(I) &= \log(m_{Al}/m_{OH}) + \log K_w^\circ \\ &= \log K_s^\circ + 2\log(\gamma_2/\gamma_1). \end{aligned} \quad (8)$$

It should be noted that  $f(I)$  is independent on the activity of water. Figure 1 gives relationships between  $f(I)$  and  $I$  which were calculated from the solubility data of gibbsite reported by Russell *et al.*<sup>2)</sup> and  $K_w^\circ$  values<sup>20)</sup> at a given temperature.

Using the extended Debye-Hückel equation with added terms, we can express the mean activity coefficient ( $\gamma_i$ ) as follows;

$$\log \gamma_i = -A_t I^{1/2} / (1 + B_t a_i I^{1/2}) - c_i I - d_i I^2, \quad (9)$$

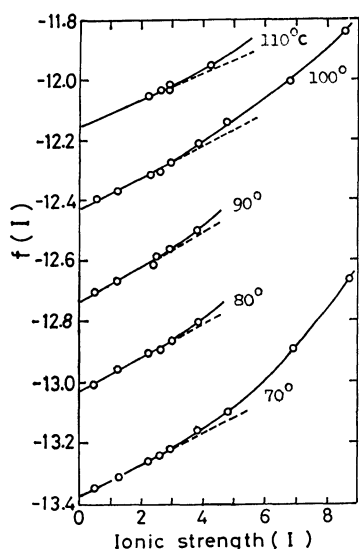
where  $A_t$  is the theoretical limiting Debye-Hückel slope,  $B_t$  a parameter depending upon temperature and dielectric constant of solvent,  $a_i$  an ion size parameter, and  $c_i$  and  $d_i$  are adjustable parameters. Substituting Eq. 9 into Eq. 8,

$$\begin{aligned} f(I) &= \log K_s^\circ + 2A_t I^{1/2} [1/(1 + B_t a_1 I^{1/2}) \\ &\quad - 1/(1 + B_t a_2 I^{1/2})] + CI + DI^2, \end{aligned} \quad (10)$$

where  $C=2(c_1-c_2)$  and  $D=2(d_1-d_2)$ . The problem is to decide the five parameters,  $K_s^\circ$ ,  $a_1$ ,  $a_2$ ,  $C$ , and

TABLE 1. TEMPERATURE DEPENDENCY OF  $K_s^\circ$ ,  $K_w^\circ$ ,  $C$ , AND  $D$ 

No.	$t/^\circ\text{C}$	Case 1				Case 2		
		$\log K_s^\circ$	$C \times 10^2$	$D \times 10^3$	$\log K_r^\circ$	$\log K_s^\circ$	$C \times 10^2$	$\log K_r^\circ$
1	40	-14.51	3.44	4.11	-0.97	-14.55	5.98	-1.01
2	60	-13.76	6.94	1.78	-0.74	-13.75	6.18	-0.74
3	70	-13.36	3.20	4.99	-0.57	-13.38	5.68	-0.59
4	80	-13.03	4.82	2.66	-0.44	-13.04	5.94	-0.45
5	90	-12.73	4.61	3.61	-0.32	-12.74	6.14	-0.33
6	100	-12.42	3.97	3.29	-0.18	-12.44	5.72	-0.19
7	110	-12.15	4.27	-0.57	-0.05	-12.22	6.80	-0.12
8	130	-11.77	5.24	5.68	0.08	-11.83	9.04	0.02
9	150	-11.54	11.18	-3.89	0.09	-11.51	9.24	0.12
10	170	-11.16	7.37	10.31	0.30	-11.26	13.71	0.20

Fig. 1. Relationships between  $f(I)$  and ionic strength( $I$ ) according to Eq. 8.

$D$  to get the best statistical fit for the data given in Fig. 1.

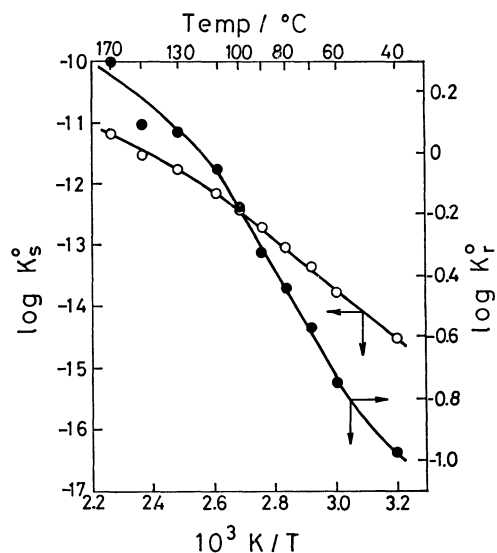
### Results and Discussion

Most of solubility measurements of gibbsite in alkaline solutions presented up to date were carried out at 25  $^\circ\text{C}$ . Lyapunov reported interesting results showing an effect of NaCl addition on the solubility of gibbsite at 60 and 95  $^\circ\text{C}$ , but the range of conditions of solubility measurements was limited.<sup>11</sup> The Russel's data seems to be the most useful solubility data of gibbsite in the range of higher temperature and NaOH concentrations. The method presented here, therefore, was applied mainly to the Russel's data.

*The Case of the Same Ion Size Parameters.* Assuming the same ion size parameters, i.e.,  $a_1 = a_2$ , as did May<sup>10</sup> or Smith,<sup>21</sup> Eq. 10 can be simplified into a following equation:

$$f(I) = \log K_s^\circ + CI + DI^2 \quad (\text{Case 1}). \quad (11)$$

Table 1 gives  $\log K_s^\circ$ ,  $C$ , and  $D$  obtained by the least square calculations for Eq. 11. Furthermore, Fig. 1 shows good straight line relationship between  $f(I)$  and  $I$  in the range of low ionic strengths, that is,

Fig. 2. Temperature dependencies of  $\log K_s^\circ$  and  $\log K_r^\circ$  from 40 to 170  $^\circ\text{C}$  for the case 1.

$$f(I) = \log K_s^\circ + CI \quad (\text{Case 2}). \quad (12)$$

Table 1 also gives the values of  $\log K_s^\circ$  and  $C$  for Eq. 12.

Figures 2 and 3 show temperature dependency of the ionic solubility product of gibbsite for the case 1 and 2, respectively. Good linear relationships between  $\log K_s^\circ$  and  $1/T$  can be observed in the range of 40–110  $^\circ\text{C}$ .

$$\log K_s^\circ = -4064/T - 1.54 \quad (\text{Case 1}), \quad (13)$$

$$\log K_s^\circ = -4032/T - 1.65 \quad (\text{Case 2}). \quad (14)$$

According to Eqs. 13 and 14, the values of  $\log K_s^\circ$  at 25  $^\circ\text{C}$  become the same value of -15.18, which is very close to the value of -15.30 reported by Kittrick,<sup>6</sup> being considerably lower than the value of -14.05 presented by May.<sup>10</sup> Based on the  $\Delta G_f^\circ$  value of -1151.9 kJ/mol selected for gibbsite by Parks,<sup>9</sup> the standard Gibbs free energy of formation ( $\Delta G_f^\circ$ ) for  $\text{Al}(\text{OH})_4^-$  ion is calculated to be -1302.5 kJ/mol. The heat of reaction of Eq. 4 was found to be 77.4–77.8 kJ between 40 and 110  $^\circ\text{C}$ , and to have a tendency to decrease at temperature above 110  $^\circ\text{C}$ .

For the following reaction of gibbsite with  $\text{OH}^-$  ion,

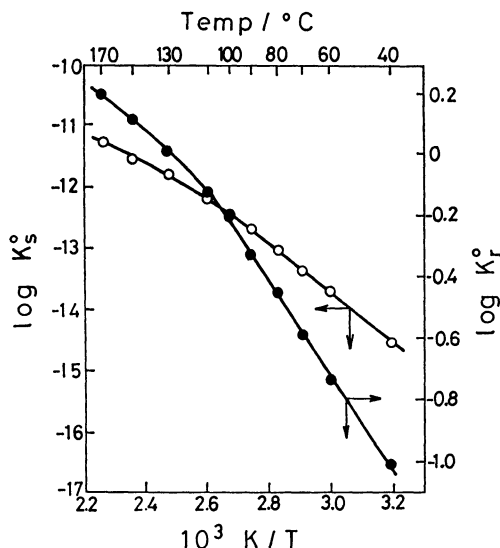
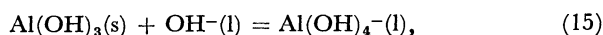


Fig. 3. Temperature dependencies of  $\log K_s^0$  and  $\log K_r^0$  from 40 to 170 °C for the case 2.



$$K_r^0 = a_{\text{Al}}/a_{\text{OH}}, \quad (16)$$

using Eqs. 5 and 7,  $K_r^0$  is given by

$$K_r^0 = K_s^0/K_w^0. \quad (17)$$

Table 1, Figs. 2 and 3 also show the values of  $\log K_r^0$ , and its temperature dependency in the range from 40 to 110 °C is given as follows;

$$\log K_r^0 = -1598/T + 4.10 \quad (\text{Case 1}), \quad (18)$$

$$\log K_r^0 = -1567/T + 3.98 \quad (\text{Case 2}). \quad (19)$$

According to Eq. 18 or 19, the heat of reaction of Eq. 15 is 30.1–30.5 kJ.

*The Case of Different Ion Size Parameters.* In order to evaluate effects of the ion size parameters,  $a_1$  and  $a_2$ , on  $\log K_s^0$ , we assumed conveniently  $c_2 = d_2 = 0$  for the dissociation of water. Then, from Eqs. 7 and 9.

$$\log (K_s/a_w) = \log K_w^0 + 2A_t I^{1/2}/(1 + B_t a_2 I^{1/2}). \quad (20)$$

Using  $K_s = m_{\text{H}} m_{\text{Al}} = K_w (m_{\text{Al}}/m_{\text{OH}})$  and Eq. 20,

$$\begin{aligned} \log (K_s/a_w) &= \log K_w^0 + \log (m_{\text{Al}}/m_{\text{OH}}) \\ &\quad + 2A_t I^{1/2}/(1 + B_t a_2 I^{1/2}). \end{aligned} \quad (21)$$

At a given temperature, the value of  $\log (K_s/a_w)$  depends upon the concentration ratio,  $(m_{\text{Al}}/m_{\text{OH}})$ , at equilibrium and the ion size parameter,  $a_2$ , for  $\text{H}^+$  and  $\text{OH}^-$  ions. Figure 4 shows plots of  $\log (K_s/a_w)$  and  $I^{1/2}/(1 + 1.51I^{1/2})$  at 70 °C with  $a_1 = 4.5$  Å and various values of  $a_2$  from 3.5 to 6.0 Å. It is obvious from Fig. 4 that  $\log (K_s/a_w)$  and slopes of curves increase with decrease in the  $a_2$  value.

On the other hand, from Eqs. 5 and 9,

$$\begin{aligned} \log (K_s/a_w) &= \log K_s^0 + 2A_t I^{1/2}/(1 + B_t a_1 I^{1/2}) \\ &\quad + 2c_1 I + 2d_1 I^2. \end{aligned} \quad (22)$$

According to the Debye-Hückel theory, generally a plot of  $\log (K_s/a_w)$  vs.  $I^{1/2}/(1 + B_t a_1 I^{1/2})$  produces a straight line at low ionic strengths with the theoretical limiting slope,  $2A_t$ , and the intercept of  $\log K_s^0$  at  $I=0$ , and the last two terms becomes important only

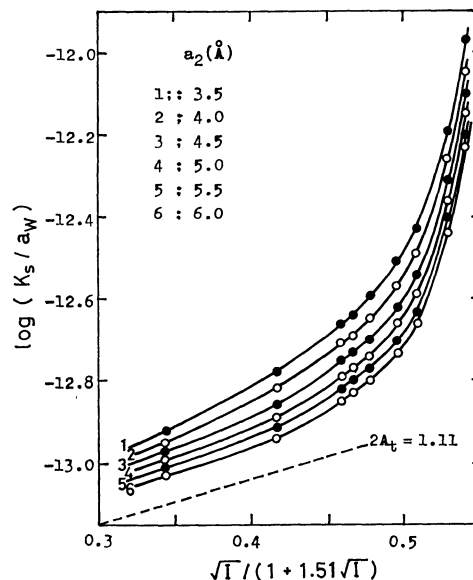


Fig. 4. Plots of  $\log(K_s/a_w)$  vs.  $I^{1/2}/(1 + 1.51I^{1/2})$  at various values of  $a_2$  in the case of  $a_1 = 4.5$  Å and 70 °C.

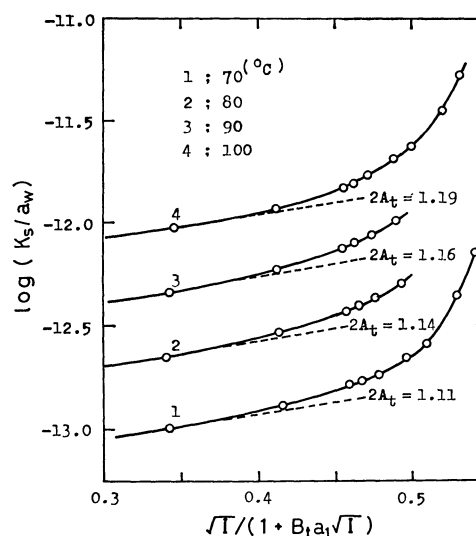


Fig. 5. Plots of  $\log(K_s/a_w)$  vs.  $I^{1/2}/(1 + B_t a_1 I^{1/2})$  at temperatures of 70, 80, 90, and 100 °C in the case of  $a_1 = 4.5$  Å and  $a_2 = 5.0$  Å.

at higher ionic strengths. Figure 5 shows a plot of  $\log (K_s/a_w)$  vs.  $I^{1/2}/(1 + B_t a_1 I^{1/2})$  at 70, 80, 90, and 100 °C in the case of  $a_1 = 4.5$  Å and  $a_2 = 5.0$  Å.<sup>24)</sup> Similarly, Fig. 6 shows a plot of  $\log (K_s/a_w)$  vs.  $I^{1/2}/(1 + B_t a_1 I^{1/2})$  at 60 °C, which were calculated from the Russell's data in NaOH solutions and the Lyapunov's data in both NaOH and (NaOH+NaCl) solutions. It is obvious from Figs. 5 and 6 that the straight line relationships hold at ionic strengths as high as 1.0, and that these slopes are very close to the theoretical values,  $2A_t$ , of 1.09, 1.11, 1.14, 1.16, and 1.19 at 60, 70, 80, 90, and 100 °C, respectively. The Lyapunov's data in NaOH and (NaOH+NaCl) solutions are able to be represented by the same curve as shown in Fig. 6, and gives  $\log K_s^0 = -13.60$  at  $I=0$ , which differs a little from a value of  $\log K_s^0 = -13.73$  for the Russell's data.

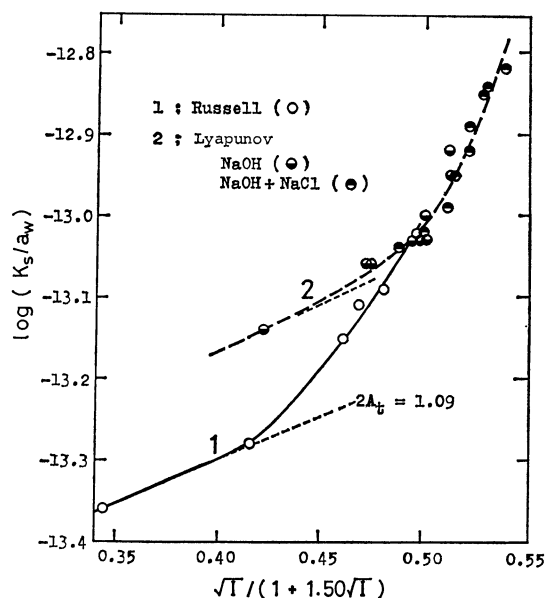
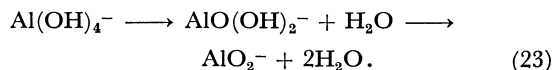


Fig. 6. Plots of  $\log(K_s/a_w)$  vs.  $I^{1/2}/(1 + 1.50I^{1/2})$  at 60 °C obtained from the Russell's data<sup>2)</sup> and the Lyapunov's data<sup>11)</sup> in the case of  $a_1 = 4.5$  Å and  $a_2 = 5.0$  Å.

At ionic strengths above 1.0,  $\log(K_s/a_w)$  shows positive deviations from the straight line. Such positive deviation at high ionic strengths was also observed in  $\text{Ca}(\text{OH})_2\text{-NaNO}_3\text{-H}_2\text{O}$ <sup>22)</sup> or  $\text{NiSO}_4\text{-CoSO}_4\text{-(NH}_4)_2\text{-SO}_4\text{-H}_2\text{O}$ <sup>23)</sup> system, and was considered to be attributed to the formation of complexes. Moolenaar concluded from Infrared, Raman, and <sup>23</sup>Na and <sup>27</sup>Al NMR spectra of sodium aluminate solutions that at aluminium concentrations below 1.5 M, the tetrahedral  $\text{Al}(\text{OH})_4^-$  ions exist as the predominant aluminium-bearing species in the solution and that at aluminium concentrations of about 1.5 M and above,  $\text{Al}(\text{OH})_4^-$  condenses to form  $\text{Al}_2\text{O}(\text{OH})_6^{2-}$  ion.<sup>19)</sup> In a detailed study of the saturated vapour pressures exerted by sodium hydroxide and aluminate solutions, Dibrov advanced evidence for the aluminate ion undergoing dehydration to the meta-aluminate ion  $\text{AlO}_2^-$  at high concentrations of 15%  $\text{Na}_2\text{O}$  and above:



From the above discussions it is reasonable to consider that the positive deviation from the straight line may be attributed to the formation of complex ion such as  $\text{Al}_2\text{O}(\text{OH})_6^{2-}$  and/or the dehydration of  $\text{Al}(\text{OH})_4^-$ , leading to decrease in the activity coefficient of aluminate ion. This presents a striking contrast

to increase in the activity coefficient designated by the salting-out effect.<sup>20)</sup> The similar application of the method presented in this paper to alumina monohydrates is currently performed with success.

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